AMENDMENTS TO THE CLAIMS

Claim 1 (Currently Amended): A process for preparing trichlorosilan ($HSiCl_3$) by catalytic hydrodehalogenation of silicon tetrachloride ($SiCl_4$) in the presence of hydrogen and a supported catalyst at a temperature in the range from 300 to 1000°C, wherein said catalytic hydrodehalogenation comprises contacting said supported catalyst with a $SiCl_4/H_2$ mixture having a molar ratio of from 1:0.9 to 1:20,

wherein said supported catalyst has a catalyst content, calculated as element, of from 0.1 to 10% by weight and comprises at least one metal or metal salt selected from the group consisting of calcium, strontium, barium, calcium chloride, strontium chloride, and barium chloride, ~~and~~

wherein said at least one metal or metal salt has been applied to a support selected from the group consisting of leached glass, fused silica, a porous siliceous support and a SiO_2 support,

wherein said catalytic hydrodehalogenation is conducted in a fixed-bed reactor, in a fluidized-bed reactor or in a moving-bed reactor, and

wherein said catalytic hydrodehalogenation is conducted at a temperature in the range from 600 to 950°C and a pressure of from 0.1 to 100 bar abs.

Claims 2-4 (Canceled)

Claim 5 (Currently Amended): The process as claimed in claim 1,

wherein the supported catalyst used has a catalyst content, calculated as element, of ~~from 0.1 to 10%~~ 1 to 8% by weight.

Claim 6 (Currently Amended): The process as claimed in claim 1,

wherein [[an]] said catalytic hydrodehalogenation comprises contacting said supported catalyst with a $SiCl_4/H_2$ mixture having a molar ratio of from ~~1:0.9 to 1:20~~ 1:1 to 1:10 ~~is brought into contact with the catalyst~~.

Claim 7 (Currently Amended): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation is conducted ~~the reaction is carried out~~ in a fixed-bed reactor~~, in a fluidized-bed reactor or in a moving-bed reactor~~.

Claim 8 (Currently Amended): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation is conducted ~~the catalytic reaction is carried out~~ at a temperature in the range from 700 to 900°C ~~600 to 950°C and a pressure of from 0.1 to 100 bar abs~~.

Claim 9 (Currently Amended): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation is conducted ~~the catalytic reaction is carried out~~ at a space velocity of from 2000 to 30000 h^{-1} and the gas stream has a linear velocity of from 0.01 to 10 m/s in the reactor.

Claim 10 (Previously Presented): The process as claimed in claim 1,

wherein $HSiCl_3$ is isolated from the product mixture or the product mixture is used further directly.

Claim 11 (New): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation comprises contacting said supported catalyst with a $SiCl_4/H_2$ mixture having a molar ratio of from 1:1.5 to 1:8.

Claim 12 (New): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation comprises contacting said supported catalyst with a $SiCl_4/H_2$ mixture having a molar ratio of from 1:2 to 1:4.

Claim 13 (New): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation is conducted in a fluidized-bed reactor.

Claim 14 (New): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation is conducted in a moving-bed reactor.

Claim 15 (New): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation is conducted at a pressure of from 1 to 10 bar abs.

Claim 16 (New): The process as claimed in claim 1,

wherein said catalytic hydrodehalogenation is conducted at a pressure of from 1.5 to 2.5 bar abs.

Claim 17 (New): The process as claimed in claim 9,

wherein said catalytic hydrodehalogenation is conducted at a space velocity of from 5 000 to 15 000 h^{-1}.

Claim 18 (New): The process as claimed in claim 9,

wherein said gas stream has a linear velocity of from 0.02 to 8 m/s in the reactor.

Claim 19 (New): The process as claimed in claim 9,

wherein said gas stream has a linear velocity of from 0.03 to 5 m/s in the reactor.